15AU62

## Sixth Semester B.E. Degree Examination, Aug./Sept. 2020 **Heat and Mass Transfer**

SCHEME

Time: 3 hrs.

**USN** 

 $\mathbf{1}$ 

 $\overline{2}$ 

Max. Marks: 80

Note: 1. Answer any FIVE full questions, choosing ONE full question from each module. 2. Use of heat transfer data hand book is permitted.

### Module-1

Explain the modes of heat transfer. a.

 $(03 Marks)$  $(05 Marks)$ 

State the laws governing three basic modes of heat transfer. **.** Derive general 3 – dimensional heat conduction equation in Cartesian co-ordinates.  $\mathbf{c}$ .

 $(08 Marks)$ 

#### OR

- Derive an expression for the temperature distribution and the rate of heat transfer for a  $\overline{a}$ hollow cylinder.  $(08 Marks)$ 
	- b. A wall is constructed of several layers. The first layer consists of brick  $(k = 0.66 \text{ w/m k})$ , 25cm thick, the second layer 2.5cm thick mortar  $(k = 0.7 \text{ w/m k})$ , the third layer 10cm thick limestone (k = 0.66 w/m k) and outer layer of 1.25cm thick plaster (k = 0.7 w/m k). The heat transfer coefficients on interior and exterior of the wall fluid layers are 5.8 w/m<sup>2</sup>k and 11.6 w/m<sup>2</sup>k respectively.

Find:

- Overall heat transfer coefficient  $i)$
- ii) Overall thermal resistance per m<sup>2</sup>
- iii) Rate of heat transfer per  $m^2$ , if the interior of the room is at 26<sup>o</sup>C while outer air is at  $-7$ °C
- iv) Temperature at the junction between mortrar and limestone.

 $(08 Marks)$ 

## Module-2

 $\overline{\mathbf{3}}$ 

Obtain an expression for temperature distribution and heat flow through a rectangular fin, a. when the end of fin is insulated.  $(08 Marks)$ 

An electronic semiconductor device has a rating of 60mw. In order to keep its proper b. operation, the inside temperature should not exceed  $70^{\circ}$ C. The device can dissipate about 20mw of heat on its own when placed in an environment at  $40^{\circ}$ C with heat transfer coefficient of  $12.5$  W/m<sup>2</sup> k. To avoid overheating of the device, it is proposed to install aluminium ( $k = 190$  W/m k) square fins 0.6mm side, 10mm long, to provide additional cooling. Find the number of fins required. Assume no heat loss from the tip of fins.

 $(08 Marks)$ 

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 $OR$ 

- 4a Explain the following with their significance
	- i) Biot number
	- ii) Fourier number<br>iii) Thermal time constant.
	- ii) Fourier number<br>iii) Thermal time constant. (06 Marks)
	- b. In a quenching process, a copper plate 3mm thick is heated upto  $400^{\circ}$ C and then exposed to an ambient at  $25^{\circ}$ C, with the convection coefficient of  $28w/m^2$ k. Calculate the time required<br>for the plate to reach the temperature of  $50^{\circ}$ C. Take thermo-physical properties as for the plate to reach the temperature of 50°C. Take thermo-physical properties as  $C = 380$  J/kg k, P = 8800 kg/m<sup>3</sup>, k = 385 W/m-k. C:  $C = 380 \text{ J/kg k, P} = 8800 \text{ kg/m}^3$ , k = 385 W/m-k. (06 Marks)
	- c. An aluminium cylinder ( $k = 210$  W/m k) 50mm in diameter and 10cm long is initially at uniform temperature of  $200^{\circ}$ C. Take h = 530 W/m<sup>2</sup>k. What is the temperature on centerline of the evolution of the content of the content of the extinction of the content of the content of the content of the content o of the cylinder after one minute?

# Module-3

5a. Explain the following:

- i) Velocity boundary layer
- ii) Thermal boundary layer.
- b. Vertical door of a hot oven is 0.5m high and is maintained at 200'C. It is cxposed to atmospheric air at 20°C. Find :
	- i) Local heat transfer coefficient half way up the door
	- ii) Average heat transfer coefficient for entire door
	- iii) Thickness of free convection boundary layer at the top of the door.

(12 Marks)

(04 Marks)

## **Similar to the COR**

- 6a. thc length of tube required to heat water from  $30^{\circ}$ C to  $50^{\circ}$ C, if the wall temperature is maintained at  $(08$  Marks) A rectangular tube,  $30 \text{mm} \times 50 \text{mm}$  carries water at a rate of 2kg/s. Determine  $90^{\circ}$ C.  $\sim$ 
	- b. In a long annulus (3.5cm ID and 5cm OD), the water is heated by maintaining the outer surface of inner tube at  $60^{\circ}$ C. The water enters at  $20^{\circ}$ C and leaves at  $34^{\circ}$ C. While its flow (08 Marks) rate is  $2 \text{ m/s}$ . Estimate the heat transfer coefficient.

## Module-4

7 a. Derive an expression for LMTD of parallel flow heat exchanger.

(08 Marks)

b. A heat exchanger is required to cool 55,000 kg/h of alcohol from 66 $\degree$ C to 40 $\degree$ C using 40,000 kg/h of water entering at  $5^{\circ}$ C.

Calculate :

- i) Exit temperature of water
- ii) Heat transfer rate
- iii) Surface area required for
	-
	- i) Parallel flow type<br>ii) Counter flow type of heat exchanger

Take overall heat transfer coefficient  $U = 580$  w/m<sup>2</sup> k

 $C_{P(\text{alcohol})} = 3760 \text{ J/kg k}$ 

 $C_{\text{P(water)}}$  = 4180 J/kg k.

(08 Marks)

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 $(08 Marks)$ 

- With neat sketch, explain the regions of pool boiling. 8  $\mathbf{a}$ .
	- A steam condenser consists of a square array of 400 tubes  $(N = 20)$  each 6mm in diameter.  $\mathbf{b}$ . The tubes are exposed to saturated steam at pressure of 0.15bar  $(T_{sat} = 54^{\circ}C)$ . The tube surface is maintained at a temperature of 25°C. Calculate the condensation rate per unit length of the tubes. The tubes are arranged horizontal in vertical tier of 20 tubes. (08 Marks)

## Module-5

Explain briefly the concept of a block body. q a.

State:  $\mathbf{b}$ .

i) Kirchoff's law ii) Wien's displacement law

iii) Plnak's law.

c. A hot water radiator of overall dimensions  $2 \times 1 \times 0.2$ m is used to heat the room at 18°C. The surface temperature of radiator is 60°C and its surface is black. The actual surface of the radiator is 2.5 times the area of its envelope for convection for which the convection coefficient is given by

$$
h_c = 1.3(\Delta T)^{3} W/m^2 k
$$

Calculate the rate of heat loss from the radiator by convection and radiation.

 $(06 Marks)$ 

define the following:  $10$ a.

- Solid angle  $i)$
- Irradiation  $\mathbf{ii}$
- iii) Radiosity
- iv) Radiation shape factor,
- b. State and explain Fick's law of diffusion.
- Calculate the following quantities for an industrial furnace (black-body) emitting radiation at  $c.$ 2650°C.
	- i) Spectral emissive power at  $\lambda = 1.2 \mu m$
	- ii) Wavelength at which the emissive power is maximum
	- iii) Maximum spectral emissive power
	- iv) Total emissive power
	- v) Total emissive power of the furnace, if it is treated as gray and diffuse body with an  $(08 Marks)$ emissivity of 0.9.

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## $(04 Marks)$  $(04 Marks)$

 $(04 Marks)$ 

 $(06 Marks)$